

Flow and Heat Transfer Analysis of a Nanofluid Along a Vertical Flat Plate with Non-Uniform Heating Using Fem: Effect of Nanoparticle Diameter

Puneet Rana and R. Bhargava

Abstract—Steady two dimensional natural convection laminar boundary layer flow of an incompressible Al_2O_3 -water nanofluid along a vertical flat plate with streamwise sinusoidal surface temperature has been investigated numerically. The resulting non-linear governing equations have been solved, using an extensively validated, Galerkin Finite Element Method (FEM) for spherical shaped nanoparticles with volume fraction upto 4%, with associated boundary conditions. Dynamic based models have been implemented, for calculating the effective thermal conductivity and dynamic viscosity of nanofluid. Heat transfer enhancement is observed and highlighted due to the presence of nanoparticles. The effects of the various other parameters are discussed to achieve better control on the rate of heat transfer.

Index Terms—FEM, Natural convection, Nanofluids, Sinusoidal temperature, Vertical flat plate.

I. INTRODUCTION

The heat transfer enhancement is one of the most important technical aims for engineering systems due to its wide applications in electronics cooling systems, next-generation solar film collectors, heat exchangers technology, and various thermal systems. Choi [1] was the first person to introduce the word “nanofluids”. Nanofluids, i.e., dilute suspensions of nanoparticles, which are typically made of metals (Al, Cu) [2], metal oxides (Al_2O_3 , SiO_2 , TiO_2) nanoparticles or nonmetals (Graphite, Carbon) nanotubes in liquids, may exhibit quite different thermal properties than the pure carrier fluids. The base fluid is usually a conductive fluid, such as water, ethylene glycol, oils, Bio-fluids, Polymer solutions etc.

The classical conductivity theory of solid-fluid suspensions used for large-size particle suspensions could not explain as to why low concentrations of nanoparticles can enhance the thermal conductivity of base fluids notably larger than the model predication. Wang et al. [3] first proposed new mechanisms behind enhanced thermal transport in nanofluids, such as particle motion and eletrokinetic effects. Xuan and Li [4] recommended several possible mechanisms for enhanced thermal conductivity of nanofluids.

Later, it was found that the effective thermal conductivity

of nanofluids depends not only on the nanostructures of the suspensions but also on the dynamics of nanoparticles in liquids at high temperature. Koo and Kleinstreuer [5] stated that the effective thermal conductivity is composed of the particle’s conventional static part and a Brownian motion part.

It is well known that power law surface temperature distributions give rise to self similar boundary layer flows [6, 7]. However, Rees [8] and Roy and Hossain [9] proposed another form of surface temperature variation, namely, sinusoidal variations about a mean temperature which is held above the ambient temperature of the fluid. This type of surface temperature may be considered to define the periodic array of heaters behind or within the wall. Recently, Saha et al. [10] studied the sinusoidal temperature variation with time on the inclined walls of the attic space and Molla et al. [11] discussed the radiation effect on natural convection flow along a vertical plate with streamwise surface temperature.

In the present paper, we study the Natural convection of Al_2O_3 -water nanofluid along the vertical plate with sinusoidal heating, using the models introduced by Li [12]. The effects of various parameters have been studied.

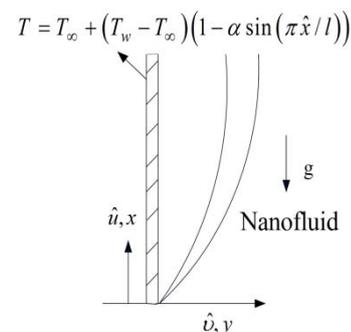


Fig. 1. Physical Model and Co-ordinate system.

II. MATHEMATICAL ANALYSIS

A steady two-dimensional laminar free convective flow from a non-isothermal semi-infinite vertical flat plate, which is immersed in an incompressible Al_2O_3 -water nanofluid, is considered. It is assumed that the heated surface temperature of the plate is maintained at the steady temperature.

$$T = T_{\infty} + (T_w - T_{\infty})(1 - \alpha \sin(\pi \hat{x}/l)) \quad (1)$$

where T_{∞} is the ambient temperature, T_w is the mean surface temperature with $T_w > T_{\infty}$, α is the relative amplitude of the

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surface temperature variations and $2l$ is the wavelength of the variations. The base fluid and the nanoparticles are in thermal equilibrium and no slip occurs between them. The coordinates system and the flow configuration are shown in Fig. 1.

The boundary layer and Boussinesq approximations are assumed to be valid. The thermo physical properties of the nanofluid are taken from [13]. The basic steady conservation of mass, momentum and thermal energy equations for nanofluids can be written in Cartesian coordinates x and y as,

$$\frac{\partial \hat{u}}{\partial \hat{x}} + \frac{\partial \hat{v}}{\partial \hat{y}} = 0 \quad (2)$$

$$\hat{u} \frac{\partial \hat{u}}{\partial \hat{x}} + \hat{v} \frac{\partial \hat{u}}{\partial \hat{y}} = \frac{1}{\rho_{nf}} \left[\mu_{nf} \frac{\partial^2 \hat{u}}{\partial \hat{y}^2} + (\rho\beta)_{nf} g(T - T_\infty) \right] \quad (3)$$

$$\hat{u} \frac{\partial T}{\partial \hat{x}} + \hat{v} \frac{\partial T}{\partial \hat{y}} = \frac{1}{(\rho C_p)_{nf}} \left[k_{nf} \frac{\partial^2 T}{\partial \hat{y}^2} \right] \quad (4)$$

where, (\hat{u}, \hat{v}) are the velocity components along the (\hat{x}, \hat{y}) axes, ρ_{nf} is the nanofluid density, μ_{nf} is the effective dynamic viscosity of the nanofluid. T is the temperature of the nanofluid, β_{nf} is the thermal expansion of the nanofluid, g is the acceleration due to gravity.

The boundary conditions are:

$$\hat{u} = \hat{v} = 0, T = T_\infty + \Delta T(1 - \alpha \sin(\pi \hat{x} / l)) \text{ at } y = 0, \quad (5a)$$

$$\hat{u} \rightarrow 0, T \rightarrow T_\infty \text{ as } y \rightarrow \infty \quad (5b)$$

To obtain the non-dimensional governing equations let us introduce the following non-dimensional variables

$$x = \frac{\hat{x}}{l}, y = Gr^{1/4} \left(\frac{\hat{y}}{l} \right), u = \frac{l}{\nu_f} Gr^{-1/2} \hat{u}, v = \frac{l}{\nu_f} Gr^{-1/4} \hat{v},$$

$$\theta = \frac{T - T_\infty}{T_w - T_\infty}, Gr = \frac{g \beta (T_w - T_\infty) l^3}{\nu_f} \quad (6)$$

where, Gr is Grashof number. $\nu_f = \mu_f / \rho_f$ is the reference kinematic viscosity, θ is the non-dimensional temperature function. Substituting the variables into Eqs (2)-(5) lead to the following non-dimensional equations, we get

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \quad (7)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = \frac{1}{(1 - \phi + \phi \frac{\rho_s}{\rho_f})} \left[\frac{\mu_{nf}}{\mu_f} \frac{\partial^2 u}{\partial y^2} + [1 - \phi + \phi \frac{(\rho\beta)_s}{(\rho\beta)_f}] \theta \right] \quad (8)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} = \frac{1}{(1 - \phi + \phi(\rho C_p)_s / (\rho C_p)_f)} \frac{1}{Pr} \frac{k_{nf}}{k_f} \frac{\partial^2 T}{\partial y^2} \quad (9)$$

and the corresponding boundary conditions are

$$u = v = 0, \theta = 1 + \alpha \sin(\pi x) \text{ at } y = 0, \quad (10a)$$

$$u \rightarrow 0, \theta \rightarrow 0 \text{ as } y \rightarrow \infty \quad (10b)$$

where Pr is Prandtl number, ϕ is the nanoparticle volume fraction. The thermophysical properties of the nanofluid, namely the density, heat capacity and volumetric expansion coefficient, have been calculated from nanoparticle and base fluid properties at the ambient temperature and are as follows [14]:

$$\rho_{nf} = (1 - \phi)\rho_f + \phi\rho_s$$

$$(\rho\beta)_{nf} = (1 - \phi)(\rho\beta)_f + \phi(\rho\beta)_s \quad (11)$$

$$(\rho C_p)_{nf} = (1 - \phi)(\rho C_p)_f + \phi(\rho C_p)_s$$

The effective thermal conductivity of the nanofluid is determined based on the models presented in [12].

III. NUMERICAL SOLUTION

The finite element method is a powerful technique for solving differential equations whether ordinary or partial as well as integral equations. The basic concept is that the whole domain is divided into various smaller elements of finite dimensions called "Finite Elements". It is the most versatile numerical technique in modern engineering analysis and has been employed to study diverse problems in heat transfer, fluid mechanics, chemical processing, rigid body dynamics, solid mechanics, electrical systems and many other fields. The steps involved in the finite element analysis are as follows:

1. Finite-element discretization
2. Generation of the element equations
3. Assembly of Element Equations
4. Imposition of boundary conditions
5. Solution of assembled equations

The assembled equations so obtained can be solved by any of the numerical technique viz. Gauss elimination method, LU Decomposition method, etc.

Before we employ the FEM, we need to reduce the aforementioned equations to a convenient set of equations. To do that, we first introduce the following transformations over the governing equation:

$$\psi = x^{3/4} f(x, \eta), \quad \eta = x^{-1/4} y, \quad \theta = \theta(x, \eta), \quad (12)$$

$$u = \partial \psi / \partial y, \quad v = -\partial \psi / \partial x$$

Substituting (12) into Eqs. (7)-(10) and after some algebraic manipulations, the transformed equations take the following form

$$\frac{1}{(1-\phi + \phi\rho_s / \rho_s)} \left\{ \frac{\mu_{nf}}{\mu_f} f''' + \left[1 - \phi + \phi \frac{(\rho\beta)_s}{(\rho\beta)_f} \right] \theta \right\} + \frac{3}{4} ff'' - \frac{1}{2} f'^2 = x \left(f' \frac{\partial f'}{\partial x} - f'' \frac{\partial f}{\partial x} \right), \quad (13)$$

$$\frac{1}{(1-\phi + \phi(\rho C_p)_s / (\rho C_p)_f)} \left[\frac{1}{Pr} \left(\frac{k_{nf}}{k_f} \right) \theta'' \right] + \frac{3}{4} f \theta' = x \left(f' \frac{\partial \theta'}{\partial x} - f'' \frac{\partial \theta}{\partial x} \right), \quad (14)$$

along with the boundary conditions

$$\begin{aligned} f(x, 0) = f'(x, 0) = 0, \quad \theta(x, 0) = 1 + \alpha \sin(\pi x), \\ f'(x, \infty) \rightarrow 0, \quad \theta(x, \infty) \rightarrow 0. \end{aligned} \quad (15)$$

The physical quantities of principle interest are the shearing stress and the rate of heat transfer in terms in terms of the skin-friction coefficient C_f and the Nusselt number Nu which can be written as

$$\begin{aligned} C_f = C_f Gr_x^{1/4} / 2 = (\mu_{nf} / \mu_f) f''(x, 0), \\ Nu = Nu Gr_x^{-1/4} = -(k_{nf} / k_f) \theta'(x, 0). \end{aligned} \quad (16)$$

Finally, the average Nusselt number is determined from:

$$Nu_{avg} = \left(\frac{1}{p} \right) \int_0^p Nu(X) dX \quad (17)$$

Here p is the length of the plate .The average Nusselt number in Eq. (17) has been evaluated numerically.

IV. RESULTS AND DISCUSSION

To provide a physical insight into the flow problem, comprehensive numerical computations are conducted for various values of the parameters that describe the flow characteristics and the results are illustrated graphically. The effect of solid volume fraction is investigated in the range of 0–4%. Also, it has been observed that if the concentration exceeds the maximum level of 8%, sedimentation takes place.

Selected computations are presented in figures 1 to 7. The ranges of the parameters are considered: $300 \leq t \leq 325$, $0.0 \leq \alpha \leq 1.0$, $0 \leq \phi \leq 0.04$, $20\text{nm} \leq d \leq 100\text{nm}$. Default parameters: Al_2O_3 -water nanofluids, $t=310\text{K}$, $\alpha=0.2$, $d=30\text{nm}$ (diameter of nanoparticles).

In order to verify the accuracy of the numerical solutions, the validity of the present numerical code has been compared with Molla et al. [11] for a limiting case ($Pr=0.7$, $\phi=0.0$) as shown in fig. 2. The three dimensional profiles for both velocity and temperature at each point on the plate have also been shown in figs. 3(a-b) keeping $d=20\text{nm}$. Moreover, an extensive mesh testing procedure was conducted to ensure a grid- independence solution of given boundary value problem.

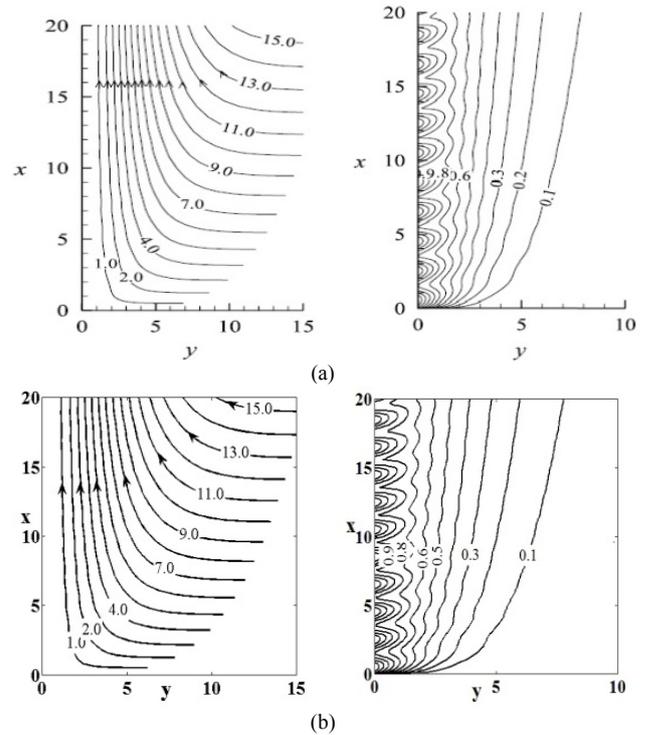


Fig. 2. (a) Streamlines and isotherms by Molla et al. [11] (b) Present FEM results.

Different combinations of meshes for both pure water and Al_2O_3 -water were also explored as shown in Table 1. In the case of Al_2O_3 -water, average Nusselt number of different nanoparticle diameter ($d=20\text{nm}$ and 100nm) has been taken into consideration. Another grid independence study was performed for Al_2O_3 -water nanofluid by varying the nanoparticle volume concentration. It has been found that a grid size of 181×101 grid points ensures the grid independent solution. The results presented here are independent of step size up to four decimal places.

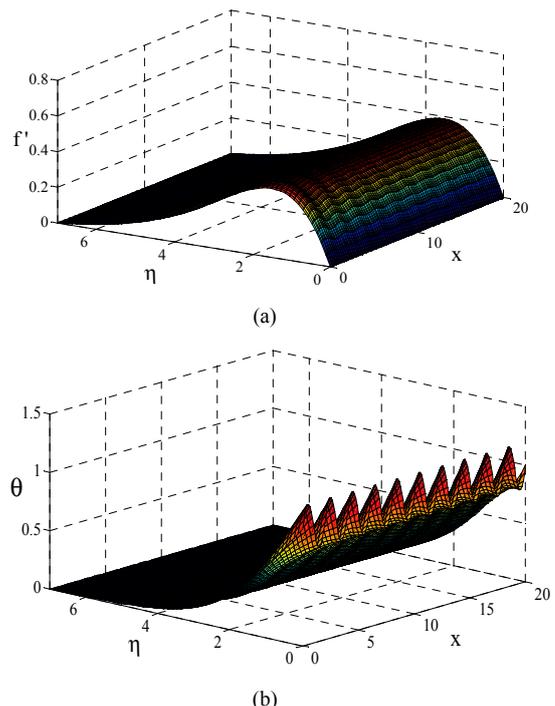


Fig. 3. 3D plots of (a) dimensionless velocity (b) dimensionless temperature for nanofluids while $\phi=0.04$, $t=320\text{K}$, $d=20\text{nm}$.

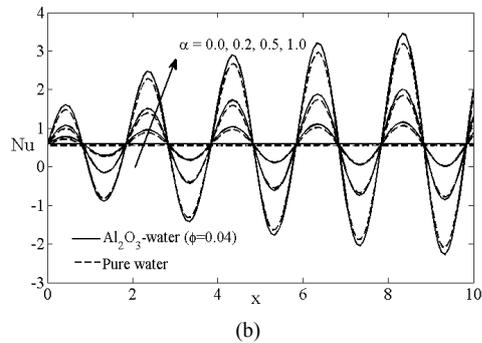
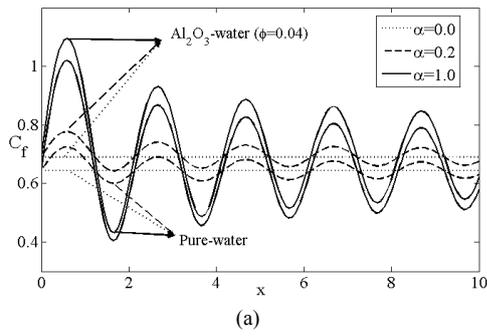


Fig. 4. (a) Skin friction coefficient and (b) Nusselt number of both Pure-water and nanofluids while $\phi=0.04$, $t=320K$.

Fig. 4 shows the skin friction and Nusselt number comparison of Al_2O_3 -water nanofluids and Pure water with different values of temperature wave amplitude on the plate for $t=320K$. It is clear from the figures that both the skin friction coefficient and the Nusselt number are uniform all over the plate if the amplitude is zero. However, with the increase of the amplitude of the heating effect both parameters also increase. The overall behaviour of these two figures may be discussed by observing the thermal and viscous boundary layers. As we know that when the temperature on the surface is relatively high, the fluids inside the boundary layer accelerate.

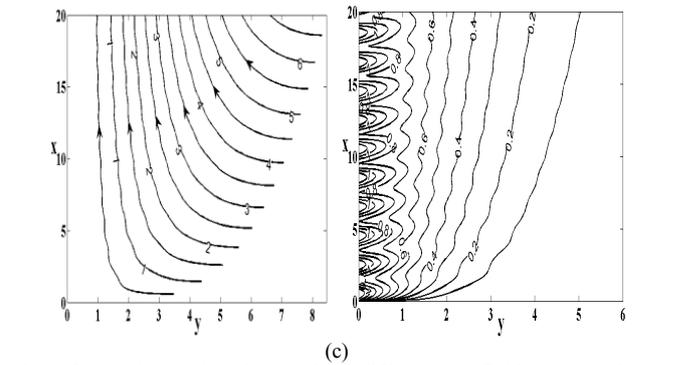
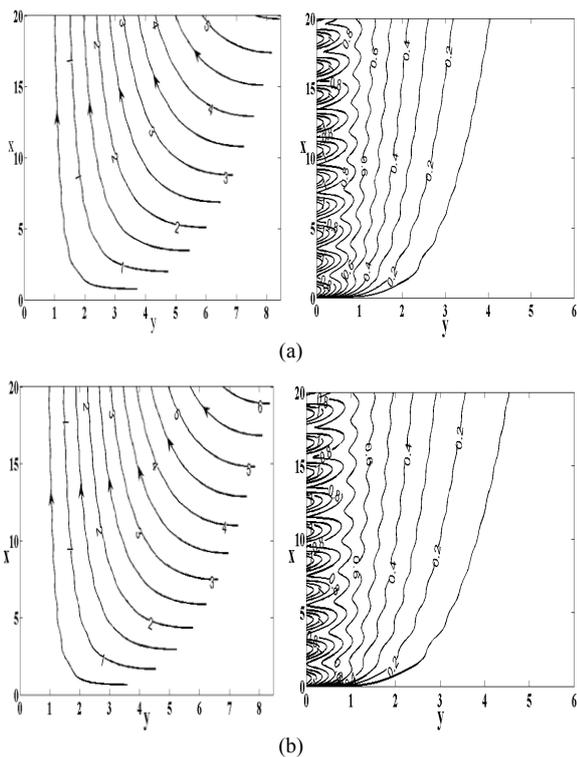


Fig. 5. Streamlines and Isotherms plot at different nanofluids temp. (a) 300K (b) 310K (c) 320K while $\phi=0.04$, $\alpha=0.2$.

On the other hand, if the surface temperature is low the fluids in the boundary layer have the minimum velocity. Therefore, it is expected that the shear stress and the rate of heat transfer will be higher at the position where the temperature is maximum. As a result the overall heat transfer will be from the fluid into the surface which can be clearly seen in Fig. 4(b) where the Nusselt number is shown as negative. The nanofluid has comparatively high skin friction and Nusselt number because of high thermal conductivity and viscosity of nanofluids as shown in Fig. 3.

Fig. 5 shows the streamlines and temperature contours for different temperatures in nanofluids with 4% nanoparticle concentration. It is seen that the streamlines concentrate near the wall as we go for higher temperature. Due to consequences of that the skin friction coefficient is higher for high temperature as shown in Fig. 7a. On the other hand the thermal boundary layer becomes thicker as the temperature increases. The flow of the nanofluid appears to be oscillating near the surface of the plate due to streamwise variations of the surface temperature.

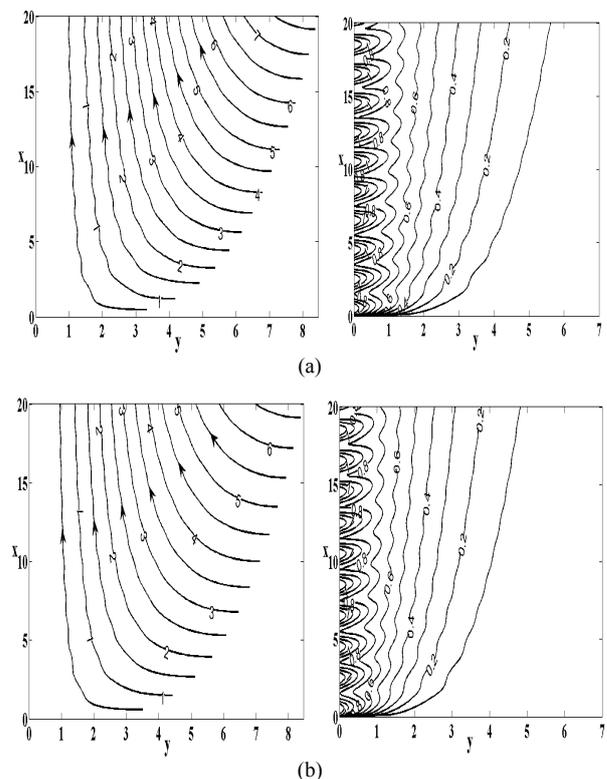


Fig. 6. Streamlines and Isotherms plot for different nanoparticle diameter (a) 20nm (b) 50nm while $\phi=0.04$, $\alpha=0.2$.

The effect of nanoparticle diameter has been shown in figs. 6 (a-b). The streamlines and temperature contours for two different nanoparticle diameter, $d=20\text{nm}$ and $d=50\text{nm}$ has been plotted. Comparatively, we found that streamline concentration and thickness of temperature contours is higher for small size nanoparticle. It can be explained on the basis of higher Brownian motion of small size nanoparticle which leads to increase the dynamic thermal conductivity.

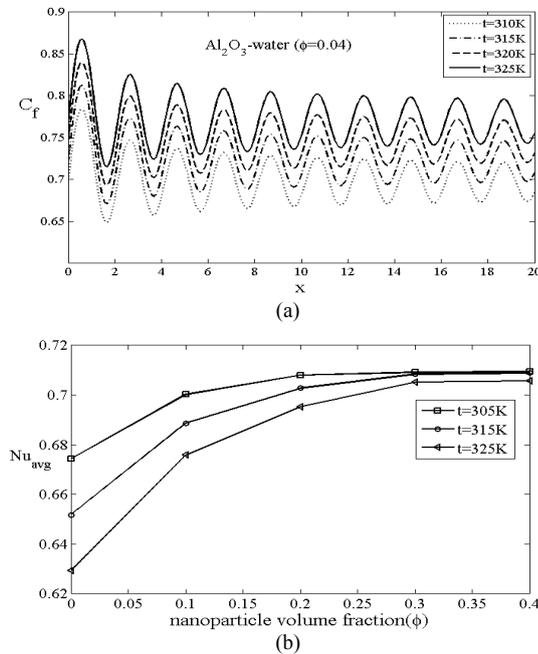


Fig. 7. (a) skin friction coefficient for different temperatures (b) Average Nusselt number with volume fraction for different temperatures.

The effect of nanoparticle volume fraction (ϕ) on average Nusselt number has been calculated for different temperatures in Fig. 7b. It is found that heat transfer increases nonlinearly with the increase with nanoparticles from 0 to 4%. It can easily be noted that this effect is almost constant from 3 to 4%. It is due to that higher concentration of nanoparticles lead to sedimentation. Moreover, the heat transfer is decreased with increase in temperature.

TABLE I: GRID INDEPENDENCE STUDY FOR A NANOFUID WITH $\phi=0.04$, $\alpha=0.2$, $t=325\text{K}$

Grid Size	Nu_{avg}		
	Pure water	Al_2O_3 -water (nanoparticle size $d=20\text{nm}$)	Al_2O_3 -water (nanoparticle size $d=100\text{nm}$)
61×21	0.585722	1.047726	0.797934
61×41	0.584432	1.043817	0.796224
81×61	0.583936	1.042091	0.795654
101×61	0.582925	1.041786	0.795015
141×81	0.582736	1.040617	0.794792
181×101	0.582663	1.040591	0.794612
201×121	0.582636	1.040571	0.794602

V. CONCLUSION

Here we have investigated the steady two-dimensional natural convection laminar flow of viscous incompressible Al_2O_3 -water nanofluid along a vertical flat plate with streamwise surface temperature. Effects of various physical

parameters arise from the governing equations and the boundary conditions on fluid flow and heat transfer have been shown. The outcomes of the results can be summarised as follows:

- ❖ Both skin-friction and Nusselt number are enhanced considerably, owing to increase in the values of the nanoparticle volume fraction,
- ❖ With the increase of the amplitude of the heating effect both skin friction and Nusselt number also increase. The effect is more pronounced with the use of nanofluids.
- ❖ Viscous and thermal boundary layers increase with the increase of ambient temperature. It is due to the increase in dynamic thermal conductivity of nanofluid with temperature.
- ❖ Different nanoparticle size can also be used to control the motion and temperature of fluid. Small sized nanoparticle has found to be high Nusselt number as compared to large sized.

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